



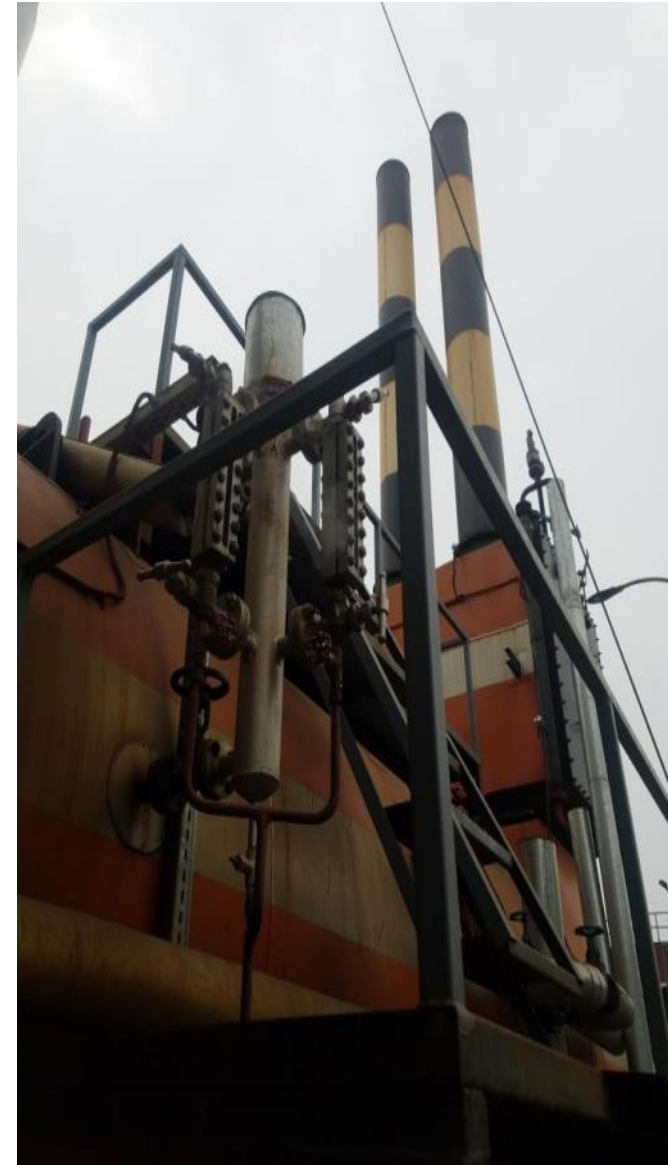
Understanding the processes and their energy  
consumption

# ENERGY EFFICIENCY IN TEXTILE UTILITIES

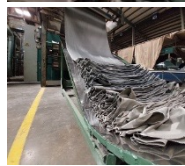
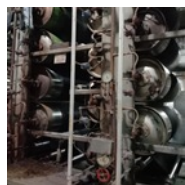
# Steam System

## Initial assessment

- STEAM BOILERS THAT ARE THE USUAL SUSPECTS:
  - Boilers that are already 20 years old
  - Fire-tube boilers with 1 or 2 passes
  - Boilers that use coal / bio mass
  - Large boilers (> 25 tons/h) that have no economizers and air preheaters
  - Fire-tube boilers and superheated steam (Must be a small installation that generates power very inefficiently)
  - Backup / Standby boilers connected with Common Steam Header
- KEY QUESTIONS TO ASK:
  - What is the temperature required in the process?
  - If its always lower than 110°C, then why are they using steam?
  - What is happening inside a boiler?



# Task!

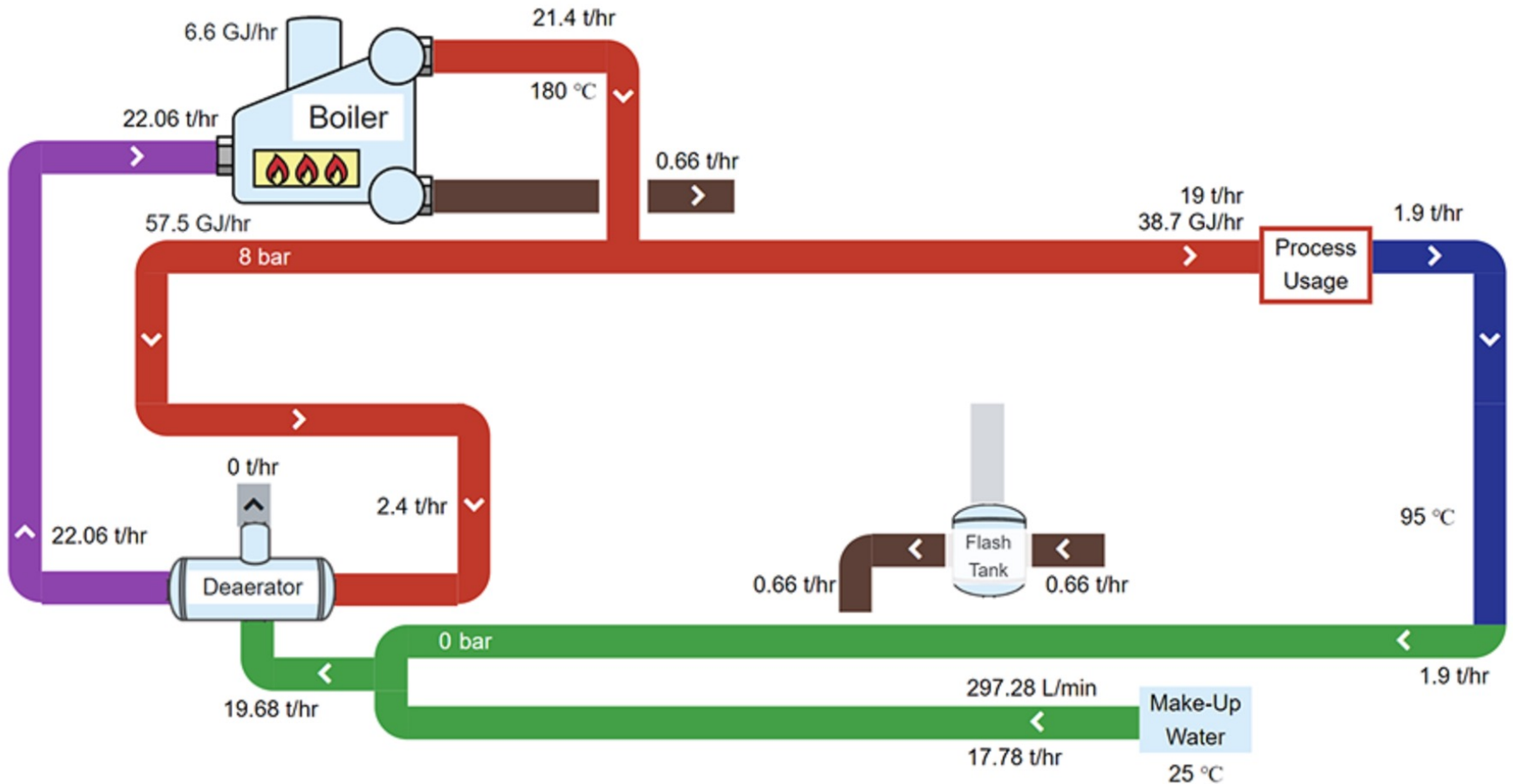


- In your groups, develop an energy flow diagram of a steam boiler
- Identify which flows need to be monitored and how
- Present your results in an “Information Market”

Time: 30 min

# Energy Balance of a Boiler

## Example: 25 TPH Coal Fired Boiler



Generated using MEASUR, a tool by US Department of Energy

# Steam System

## Boiler Efficiency Analysis

Question: Why are efficiency values different in both charts?

- Automated Air:Fuel ratio controllers help achieve much higher efficiency compared to damper controlled systems
- Flue gas temperatures as low as 110 °C are achievable on gas and liquid fuel boilers; 120-130 °C on solid fuels depending upon dew point.

| Steam Production                   |                        | Specific Energy Consumption |                         |
|------------------------------------|------------------------|-----------------------------|-------------------------|
| No. of Boilers                     | Total Steam Production | Specific Fuel Consumption   | Hourly Fuel Consumption |
| 1                                  | 66.00<br>Ton/d         | 2.63<br>mmBtu/Ton           | 0.72<br>mmBtu/h         |
| Net Energy Requirement             |                        | Daily Energy Input          |                         |
| 144.55                             | 173.70                 | 0.11                        | 1718.58                 |
| mmBtu/d                            | mmBtu/d                | MPKR/d                      | PKR/Ton                 |
| Overall Efficiency of Steam Boiler |                        |                             |                         |
| 83.2%                              |                        |                             |                         |

| Parameters | Units  | Standard | Low Fire | 25% damper | 50% damper | High Fire |
|------------|--------|----------|----------|------------|------------|-----------|
| O2         | %      |          | 3.34%    | 1.75%      | 3.04%      | 1.48%     |
| CO         | ppm    | PEQ: 649 | 1044     | 8367       | 3758       | 7570      |
| NOx        | ppm    | PEQ: 195 | 49       | 86         | 54         | 49        |
| NO         | ppm    |          | 49       | 86         | 54         | 49        |
| CO2        | %      |          | 9.93%    | 10.26%     | 9.88%      | 10.47%    |
| Excess Air | Liters | 14.7     | 17.346   | 15.729     | 16.905     | 15.435    |
| SO2        | ppm    |          | 0        | 0          | 0          | 145       |
| Flue Temp. | °C     |          | 211      | 241.1      | 259.5      | 219.6     |
| Efficiency | %      | 85%      | 81.6     | 78.5       | 78.7       | 79.7      |
| Dew Point  | °C     |          | 58.4     | 60.1       | 59         | 60.1      |
| Amb. Temp  | °C     |          | 28       | 29.2       | 29.9       | 27.9      |

# Steam System

## Boiler Efficiency Analysis

- Coal (Proximate and/or Ultimate) and ash analysis reveal a lot about fuel quality and burning efficiency

| Coal Analysis   |                  |
|---|------------------|
| Fixed carbon  | 51.21%           |
| GCV   | 5914 kCal/kg     |
| Ash Analysis  |                  |
| Unburnt carbon  | 15.47%           |
| GCV of ash  | 1412 kCal/kg     |
| Total ash residue   | 18%              |
| Saving Potential  |                  |
| Total Efficiency loss = Total ash collected per kg of coal fired x GCV of Grate Ash / GCV of Coal Fired | <b>CALCULATE</b> |



# Steam System

## Boiler Efficiency Analysis

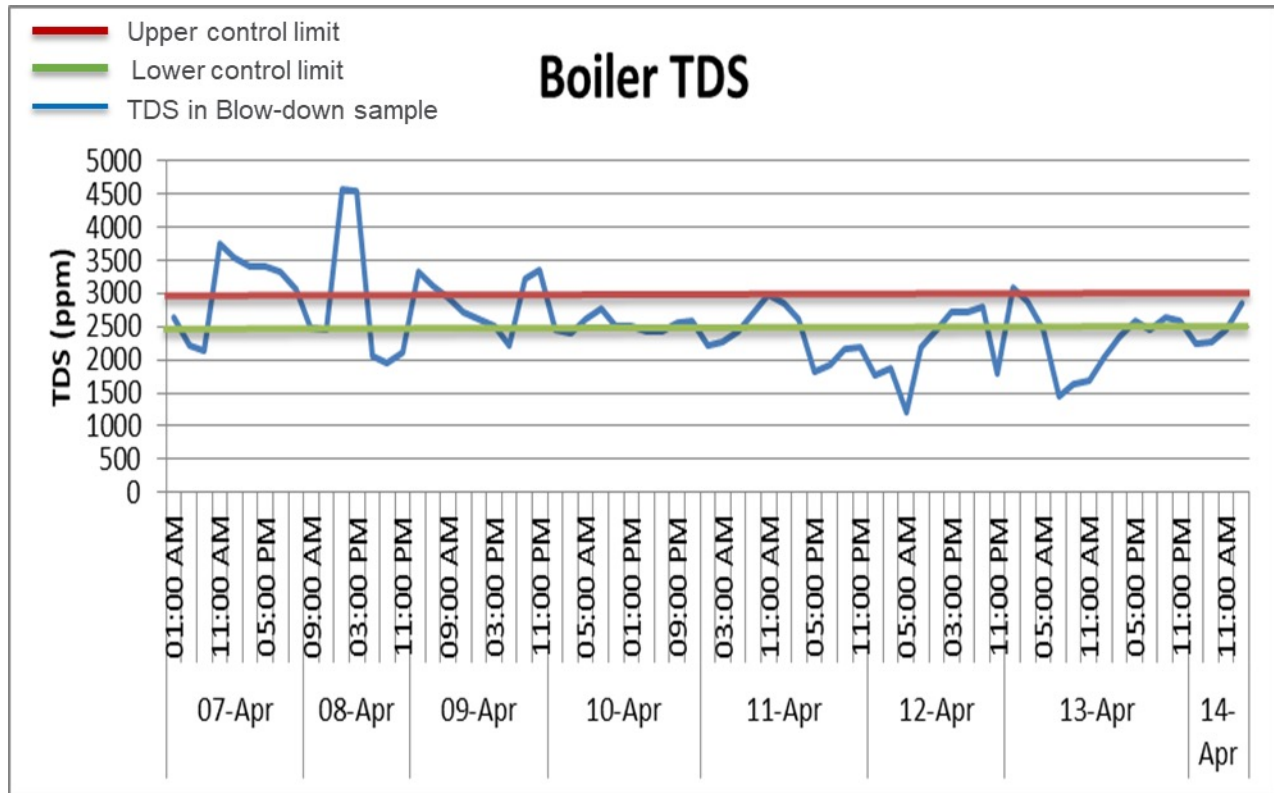
- Coal (Proximate and/or Ultimate) and ash analysis reveal a lot about fuel quality and burning efficiency

| Coal Analysis   |                 |
|---|-----------------|
| Fixed carbon  | 51.21%          |
| GCV   | 5914 kCal/kg    |
| Ash Analysis  |                 |
| Unburnt carbon  | 15.47%          |
| GCV of ash  | 1412 kCal/kg    |
| Total ash residue   | 18%             |
| Saving Potential  |                 |
| Total Efficiency loss = Total ash collected per kg of coal fired x GCV of Grate Ash / GCV of Coal Fired | 5.4%            |
| Allowance for Unburnt Carbon  | 5% (Ideally 0%) |
| Possible efficiency improvement   | <b>3.7%</b>     |

# Steam System

## Boiler Efficiency Analysis

- An automated blow-down system significantly reduces loss of steam and water





# Steam System

## Typical network issues

- Pressure drop study may reveal losses in the system due to piping network.
  - Often, high system pressure is maintained to compensate such losses
  - Need for installing Pressure Reducing Valves
- Wastage of condensate
  - Distance to boiler
  - Contamination in condensate
- Lifted Condensate lines (without pumps) resulting in back pressure on steam traps
- Flash steam at condensate recovery tank meaning that the steam traps are not functioning properly.

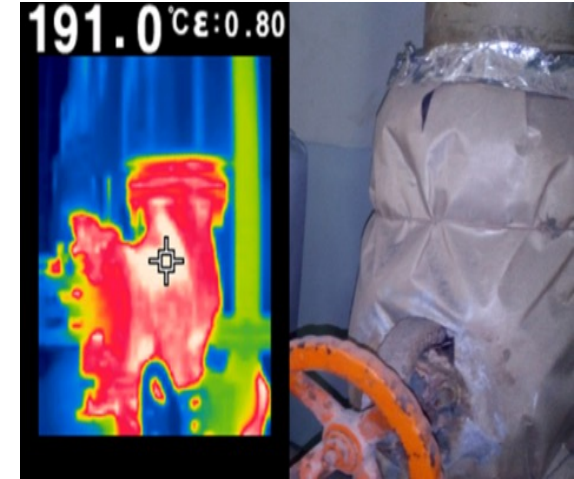
| Location   | Pressure [Bar] |
|------------|----------------|
| Boiler     | 9              |
| Washing    | 7              |
| Dryers     | 7              |
| PD Washing | 7              |



# Steam System

## Typical network issues

- Steam pressure and temperature gauges missing at important consumers
- Undersized condensate return lines
- Absence of Pressure Reducing Valves (PRVs) – every consumer is supplied same pressure
- Leakages in steam network – usually Valves and link pipe joints
- Uninsulated surfaces (pipes, valves) resulting in condensation while distribution and results derating of distribution network.
- Leakages in steam network – usually Valves and link pipe joints
- Using condensate in WHRBs – Useless as it reduces heat recovery from flue gases



# Thermal Oil Heater

## Flue Gas

### KEY QUESTION TO ASK:

- Why do you need thermal oil when you already have steam boilers?
- What is the required temperature at demand side?



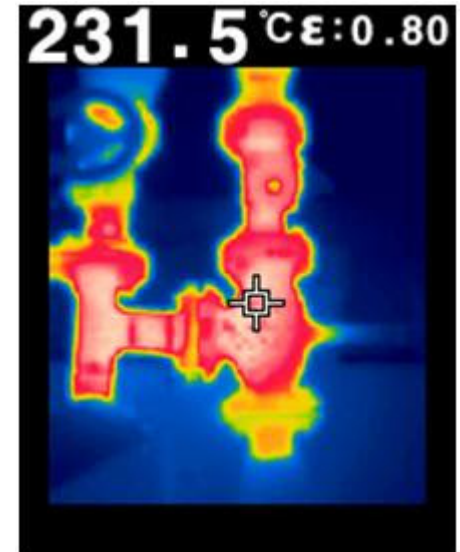
# Thermal Oil Heater

## Typical Issues

- Efficiency issues similar to boilers e.g.
  - Air-Fuel ratio (Excess oxygen)
  - Waste heat in flue gas
  - Working mode (Full Fire, High/Low Fire modes, Modulating)

**Caution: Cross check optimum excess oxygen from equipment manufacturer**

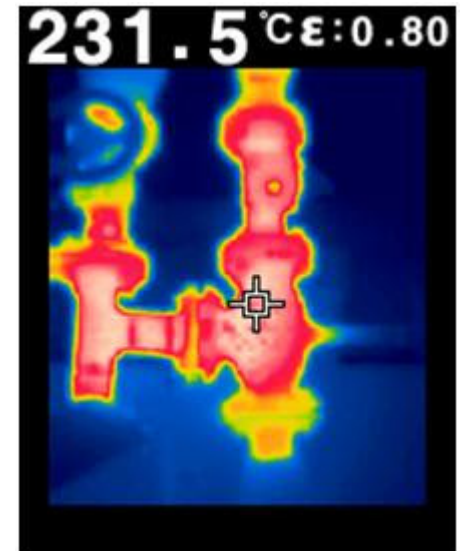
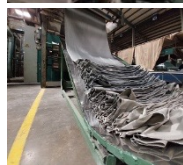
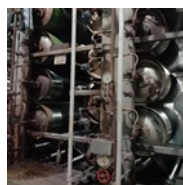
- Uninsulated surfaces, (Lengths, fittings, valves)
- Oil temperature kept too high compared to demand
  - e.g. oil temperature must be  $\sim 50$  °C higher than required temperature at Stenter
  - How to check: very low temperature difference between heated and returning oil



# Thermal Oil Heater

## Typical Issues

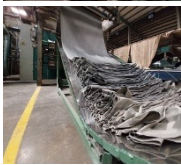
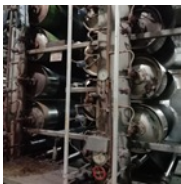
- Safety is the biggest concerns of these oil heaters.
- Always check if oil heaters are inspected on annual basis like boilers
  - In Pakistan these are not inspected as these are not considered as pressure vessels by law
  - Many accidents have been observed recently



# Power Generation

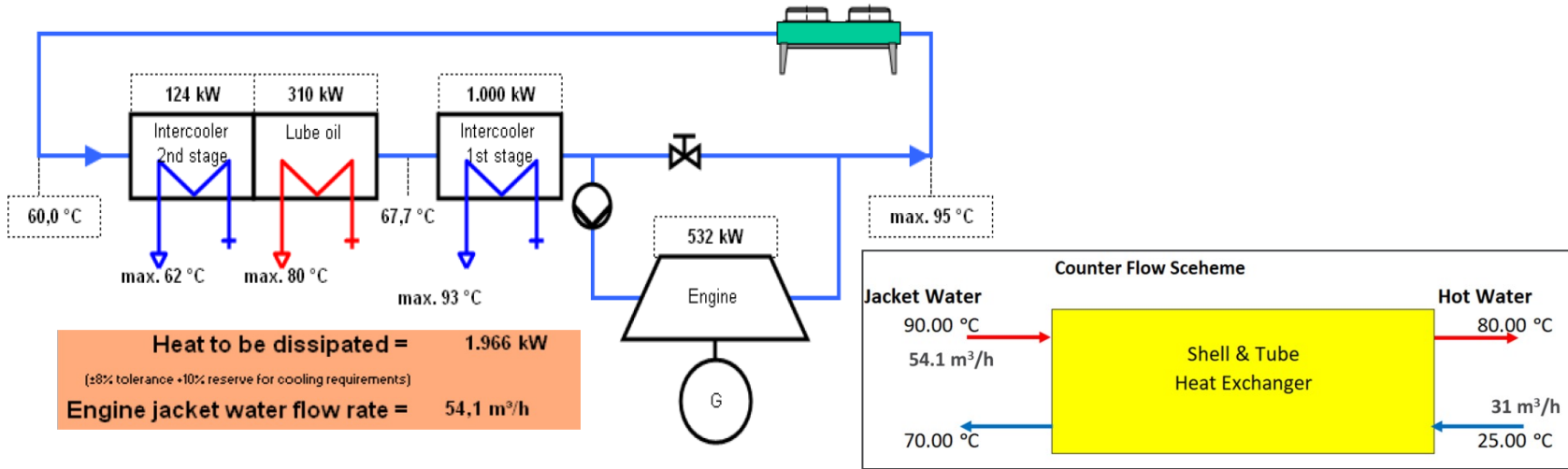
## Waste Heat Recovery

- Generating steam from engine exhaust using Waste Heat Recovery Boiler (WHRB)
- Recover heat from WHRB using a condensing economizer
- Recover heat from Jacket Water to operate an absorption chiller or supply hot water for system results in significant thermal energy saving



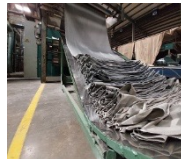


# Jacket Water Heat Recovery - Example



|   |                         |
|---|-------------------------|
| Jacket Water Flow (3.4 MW Engine)       | 54.1 m³/h               |
| Energy in Jacket Water Circuit          | 1,966 kW                |
| Recoverable energy                      | 7.1 GJ/h                |
| Steam reduction                         | 2.17 Tonne/h            |
| Coal Saving                             | 1,883 Tonne/y           |
| Financial Saving                        | 235,407 USD/y           |
| Investment for JWHR                     | 157,895 USD             |
| O&M JWHR                                | 3,158 USD/y             |
| Investment for Cooling tower automation | 8,000 USD               |
| Total Investment                        | 165,894 USD             |
| Net Savings                             | <b>232,249 USD/y</b>    |
| Payback                                 | <b>9 months</b>         |
| GHG emission reduction                  | <b>3,938 TonneCO2/y</b> |

# Waste Heat Recovery Boiler - Example



|                                 |                         |
|---------------------------------|-------------------------|
| WHRB Capacity (example)         | 2.0 TPH                 |
| Recoverable energy              | 1,393 kW                |
| Steam generation                | <b>1.7 TPH</b>          |
| Coal Saving @ GCV 6,200 kCal/kg | 206 kg-coal/h           |
| Coal Saving                     | 1,483 Tonne/y           |
| Financial Saving                | 185,329 USD/y           |
| O&M WHRB                        | 1,579 USD/y             |
| Investment for WHRB             | <b>78,947 USD</b>       |
| Net Savings                     | <b>183,751 USD/y</b>    |
| Payback                         | <b>6 months</b>         |
| GHG emission reduction          | <b>3,100 TonneCO2/y</b> |

# Waste Heat Recovery Economiser - Example



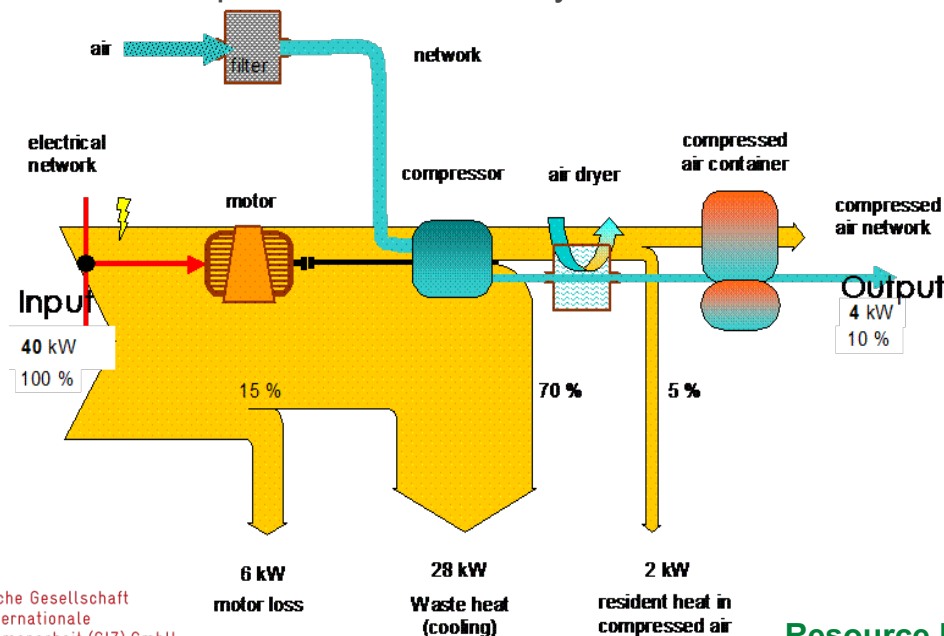
|                              |                                  |
|------------------------------|----------------------------------|
| Flu temperature (after WHRB) | 155 °C                           |
| Desired flue temperature     | <b>100 °C</b>                    |
| Desired dT                   | 55 °C                            |
| Available energy             | 235.8 kW                         |
| Raw water temperature T1     | 25.0 °C                          |
| Hot water temperature T2     | 90.0 °C                          |
| Hot water dT                 | 65.0 °C                          |
| Hot water flow rate          | <b>3.1 m<sup>3</sup>/h</b>       |
| Steam saving                 | 1,456 Tonne/y                    |
| Coal saving                  | 176 Tonne/y                      |
| Financial Saving             | <b>21,957 USD/y</b>              |
| Investment                   | <b>19,737 USD</b>                |
| Payback                      | <b>11 months</b>                 |
| GHG emission reduction       | <b>367 TonneCO<sub>2</sub>/y</b> |

- It is advisable to feed warm water (boiler feed water at 70°C) otherwise the tubes will go under thermal shock. The output temperature is normally above 95°C if fed at 75°C.
- Hot water flow rate must be according to the need of hot water at demand side

# Compressed Air System

## Waste Heat Recovery

- ~85% energy in a compressor is wasted in form of heat through the cooling circuit and only ~10% is converted into useful energy in form of compressed air
- A heat recovery system (parallel oil circuit) may provide return on investment in about 1 year
  - Important to keep automated stand-by cooling towers in case of failure in waste heat recovery system
  - Installing such system with individual compressors may increase investment but provides better safety and control



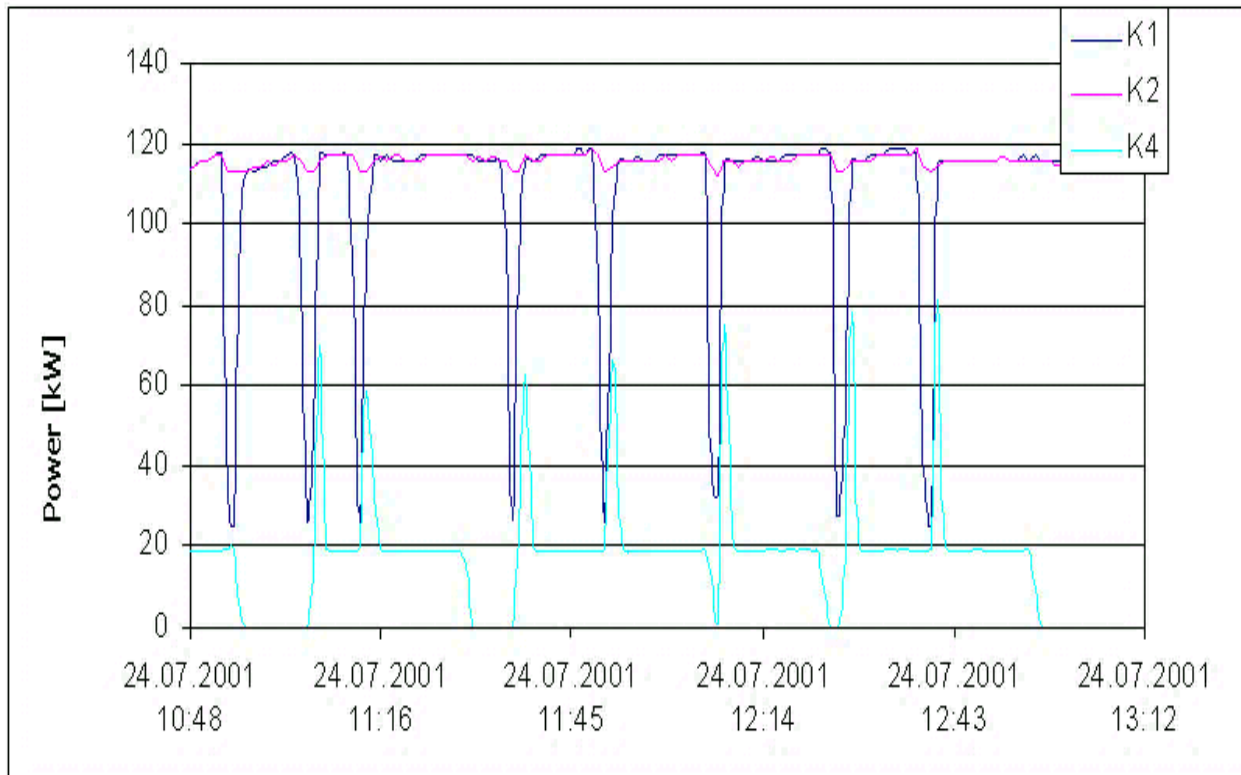
### Key Question:

- What is compressed air used for?
- Why is it necessary?

# Compressed Air System

## Load Profile

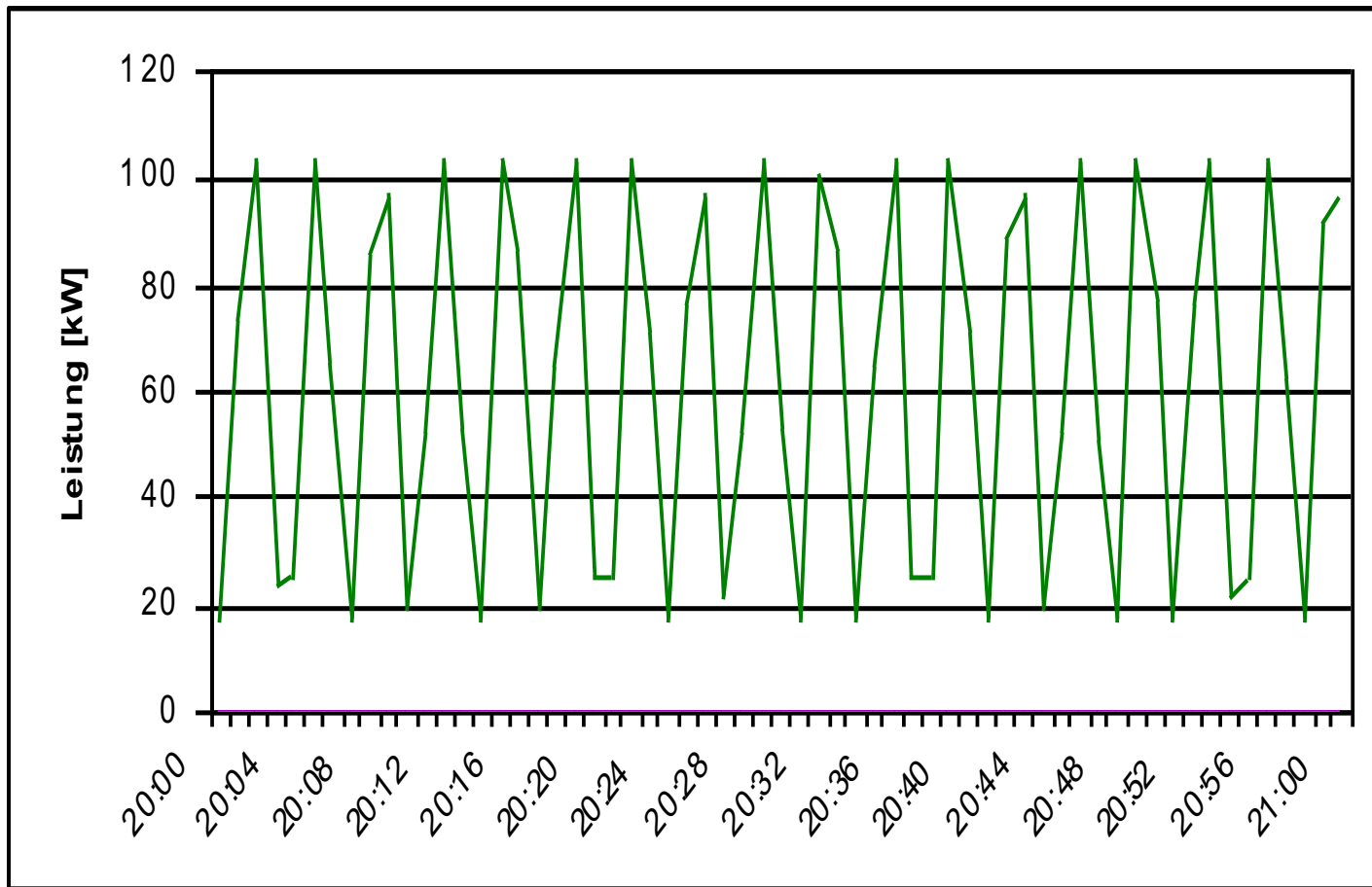
- What do you see in this chart?
- What are possible control options?



Source: ConPlusUltra

# Compressed Air System

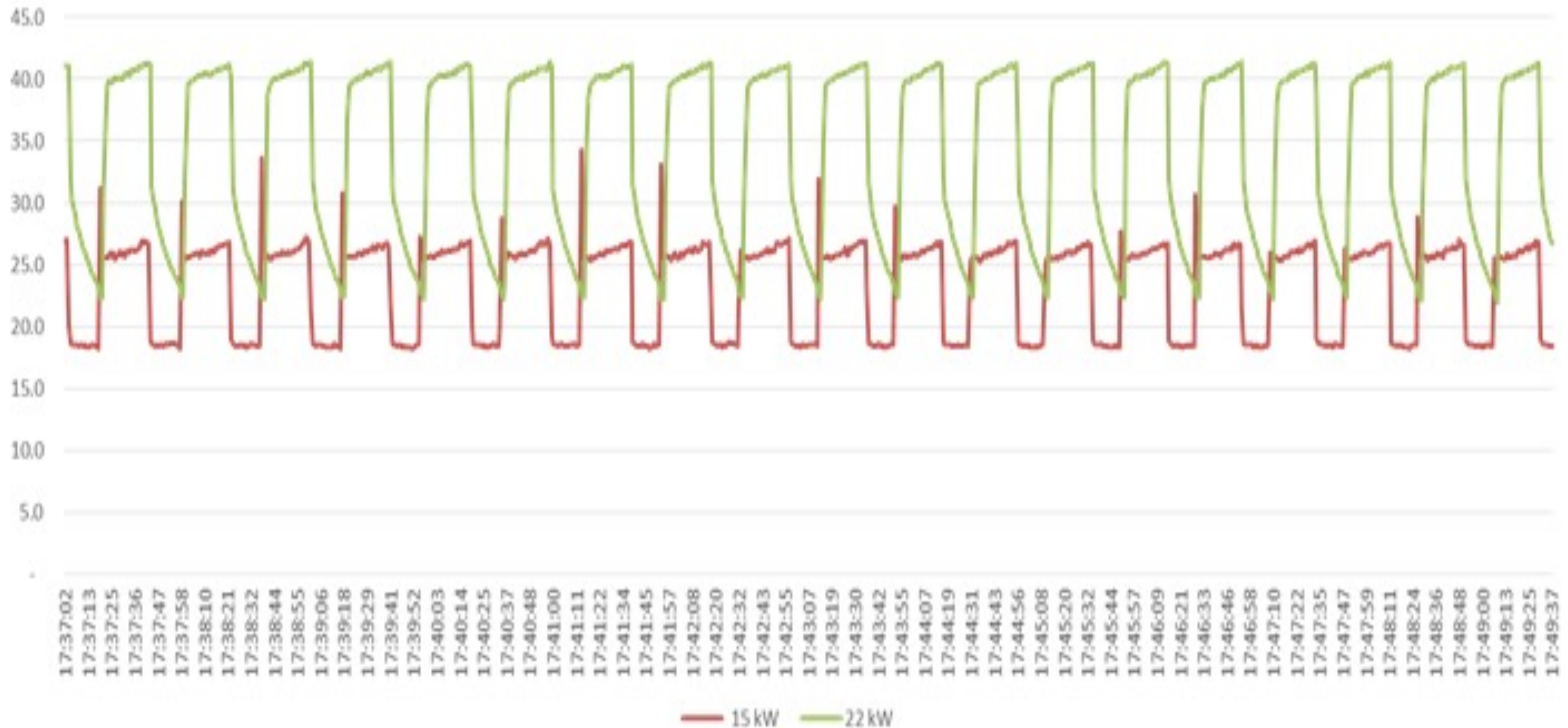
## Load Profile



Source: ConPlusUltra



# Compressed Air System Load Profile



- Compressor control automation may result in 30-50% energy saving
- Typical payback < 1 year

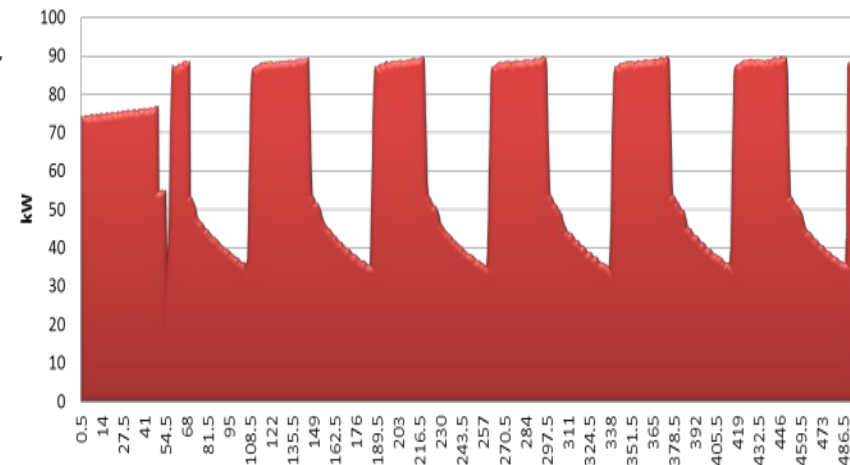
# Compressed Air System

## Network issues to be addressed

- Leakages may amount to 15-20% of total air demand; at times, leakages as high as 50% of demand have also been observed
- Faulty condensate drains and pressure regulators are one of the biggest contributors
- These leakages create artificial demand and require higher pressure set-points at compressor



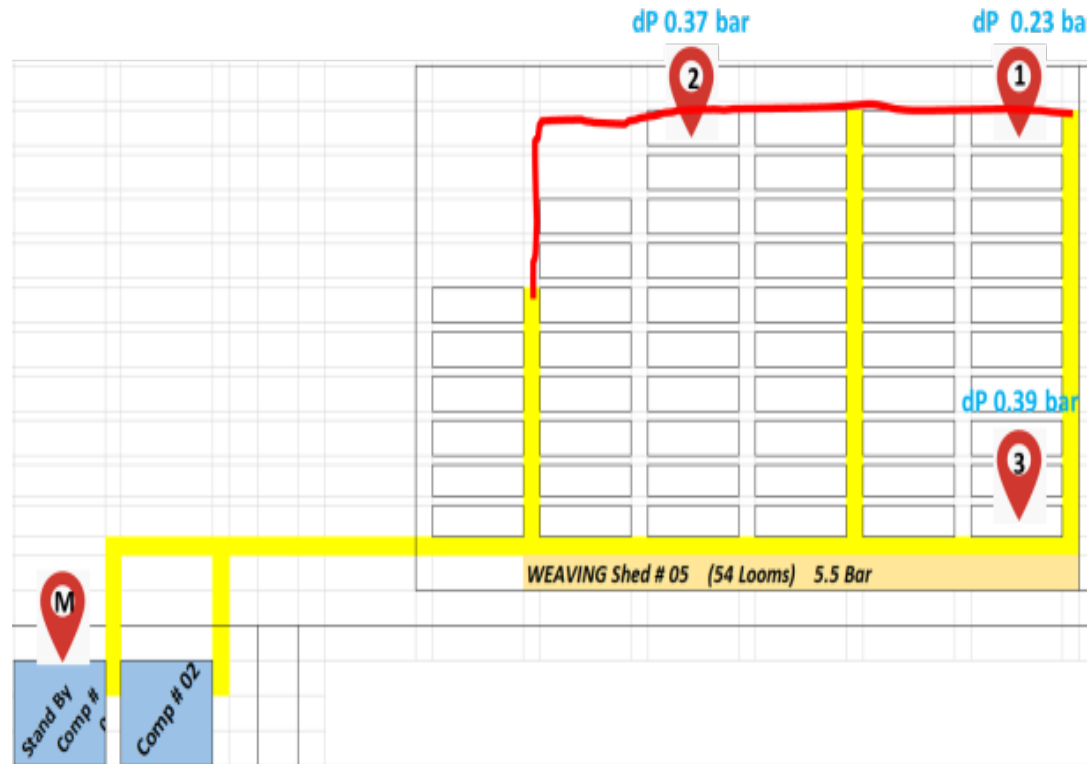
Leakage Test 28.10.2013



# Compressed Air System

## Network issues to be addressed

- Pressure drops can be reduced by using closed loop system
- Matching supply and demand air pressure reduces air consumption and leakages
- Properly sized Receiver Tank can also improve stability of system



# Compressed Air System Dryers

- Keep Dew Point between 3-5 °C to avoid condensation in the network
- Very low dew point value represents potential to reduce number of dryers
- Investment: installation of Dew point sensors
- Typical payback less than 1 year

| Name of Dryer                              | Dew Point           |
|--|---------------------|
| Main discharge                             | <b>1.5 °C</b>       |
| Dryer 1                                    | <b>0.7 °C</b>       |
| Dryer 2                                    | <b>0.4 - 0.5 °C</b> |
| Dryer 3                                    | 2.4 – 2.5 °C        |
| Dryer 4                                    | <b>24.5 °C</b>      |
| Dryer 5                                    | <b>10.1 °C</b>      |
| Dryer 6                                    | <b>10.4 °C</b>      |
| Measurements using a dew point data logger |                     |

# Cooling Towers

- Monitor heat exchange at cooling tower and modulate / sequence accordingly (In relation to range and approach temp)
- Automated control (PLC), VFDs on all pumps and fans, and temperature sensors
- The savings are escalated due to;
  - Variation in temperature during the 24 hrs
  - Seasonal variation in average temperature
  - Variation in cooling demand
- Return on investment = ~3 years

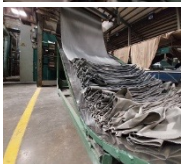
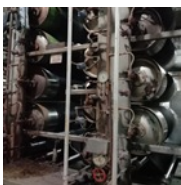


| Cooling Tower No. | Water Temperature at Inlet (°C) | Water Temperature at outlet (°C) | Range $\Delta T$ (°C) | Observations / Remarks   |
|-------------------|---------------------------------|----------------------------------|-----------------------|--|
| 1                 | 42.6                            | 35.7                             | 6.9                   | Uneven distribution of water droplets across the fills was observed that may cause the lower range |
| 2                 | 42.6                            | 35.4                             | 7.2                   |  |
| 3                 | 42.6                            | 33.7                             | 8.9                   | Satisfactory range   |
| 4                 | 42.6                            | 33.2                             | 9.4                   | Satisfactory range   |

# Cooling Towers

## Water Quality

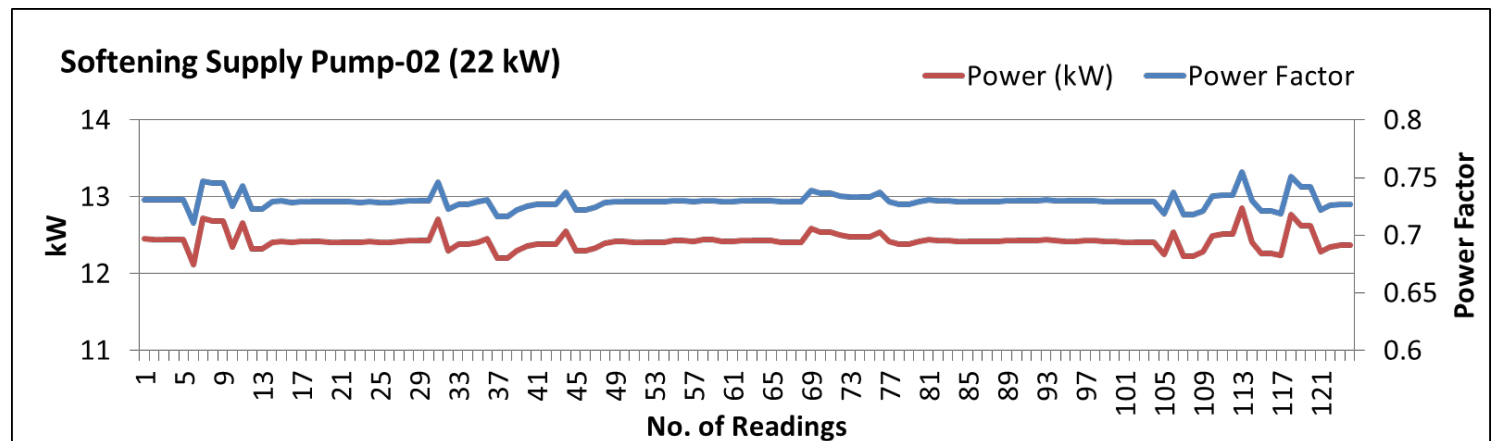
- Use soft water to makeup the water level in cooling towers
- Engineering Benefits
  - Low Scaling of Fills
  - Better heat exchange rate
- Financial Benefits
  - Decreased water pumping cost
  - Decreased water treatment chemical use
  - Low maintenance cost of cooling towers





# Pumps

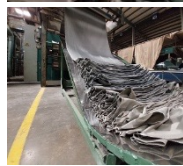
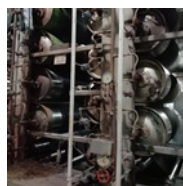
- Average pumping efficiency in manufacturing plants can be less than 40%; with many pumps operating below 10% efficiency.
- Oversized pumps and the use of throttled valves are major contributors to the loss of efficiency.
- Energy savings of 30% to 50% in pumping systems could be realised through equipment or control system changes.
- Efficiencies of 50% to 60% or lower are quite common.



# Pumps

## Typical issues to consider in pump selection

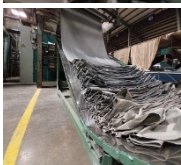
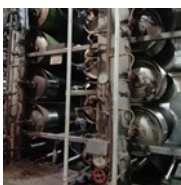
- Select pump size appropriate to the load for optimum efficiency. Avoid purchasing of oversized or undersized pumps. Evaluate Net Positive Suction Head for your system prior to ordering for a Pump.
- Select the pump type appropriate to the requirement i.e. axial, centrifugal etc. with right impeller size.
- Ensure that the selected pump is compatible with variable-speed drives.
- Ensure basic instrumentation of pumps [e.g. pressure gauges, flow meters, energy meters, etc.]
- Reduce system resistance by pressure drop assessment and selection of right pipe size and material.
- Optimize the plant design and pipe layout to minimize pumping need and pressure losses. Maximize the pipe diameter.
- Develop purchasing specifications of all pumps, including criterion to judge energy performance.
- Setup multiple sized pumping system for varying flows.



# Pumps

## Typical issues to consider in pump use

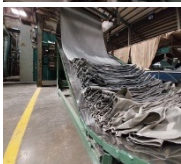
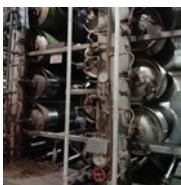
- Conduct water balance analysis to identify wastages
- Ensure that the pumping demand is reduced and system has a low required flow rate.
- Ensure that the operating pressure of the pumping system is kept low.
- Optimise number of stages in multi-stage pump in case of head margins.
- Increase fluid temperature differential to reduce pumping rates in case of heat exchangers.
- Adapt to wide load variation with variable speed drives or sequenced control of multiple pumping units.
- In the case of over designed pump, provide variable speed drive, or downsize / replace the impeller / Impeller Trimming or replace it with the correct sized pump for efficient operation.
- Use booster pumps for small loads that require higher pressures or higher heads.



# Pumps

## Typical issues to consider in pump maintenance

- Regularly monitor pumping efficiency and energy performance of pumping system.
- Monitor vibration of pumps periodically
- Monitor differential head and temperature rise across the pump (also known as thermodynamic monitoring).
- Perform distribution system inspection for scaling or contaminant build-up.
- Monitor leaks in pumps regularly and immediately fix identified leaks.
- Avoid Cavitation
- Conduct bearing inspection for increased noise and repair / replace based on conditions.
- Put pressure or flow sensors in the location that will help ensure process requirements are met without excess pumping energy.
- Replace worn impellers, especially in caustic or semi-solid applications.
- Inspect pumps for wear in seals, rings, impellers and bearings and take immediate corrective and preventive measures.



# Chillers

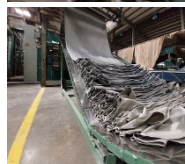
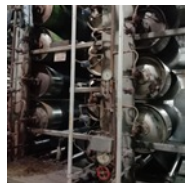
- Used in textile industry to cool down;
  - Process Water (e.g. for some dye preparation)
  - Machine cooling
  - Space cooling (in combination with ventilation system)
- Typical questions to ask;
  - Why is chilling needed?
  - What is the REQUIRED temperature?
  - Does temperature demand vary?



# Chillers

## Typical issues

- Temperature monitoring
  - Automated Modulation of chillers and cooling towers according to varying temperature needs
- Refrigerant quantity to be optimized
  - Refrigerant leakage → GHG emissions, Energy Loss
  - Consider Switching to refrigerant with low global warming potential (GWP)
  - Monitor refrigerant pressure to ensure ~ZERO Leakage
- Heat exchanger performance to be monitored
  - 20% reduction in condenser water flow → 5% increase in energy demand
- Right-sizing

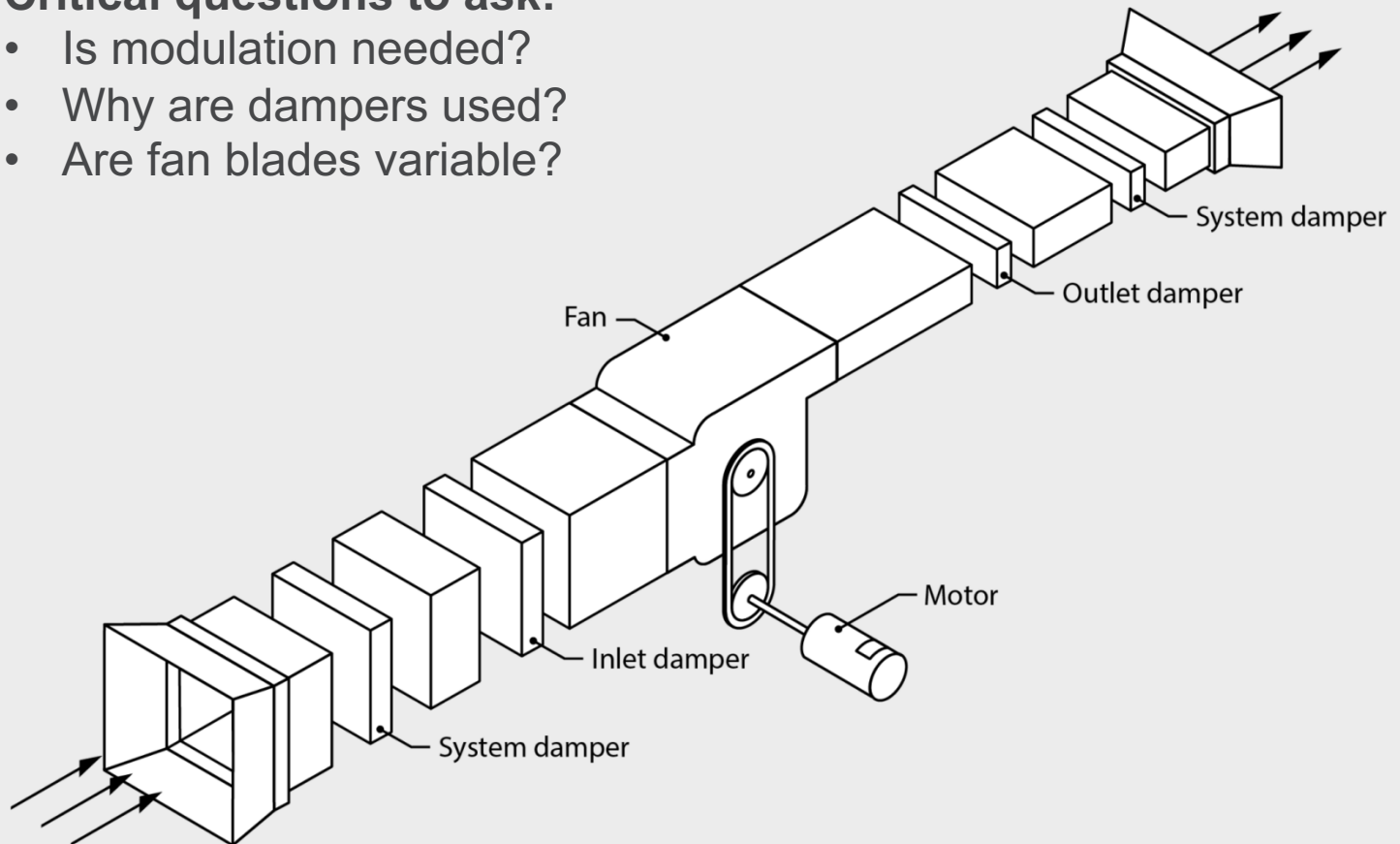




# Fans

## Critical questions to ask:

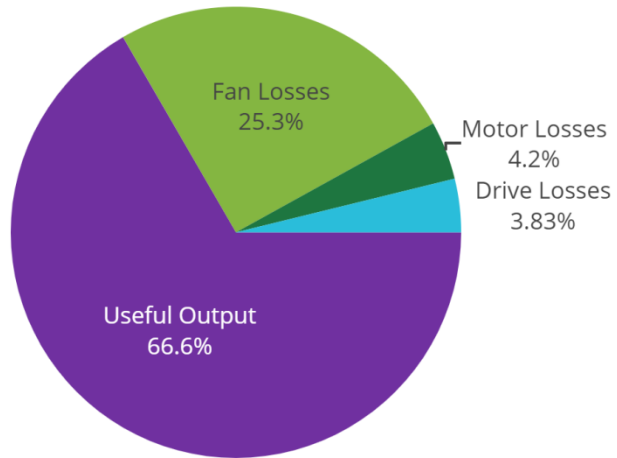
- Is modulation needed?
- Why are dampers used?
- Are fan blades variable?



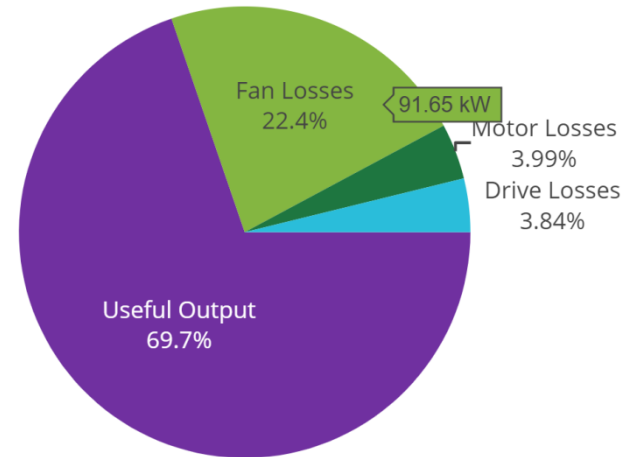
Source: MEASUR

# Fans

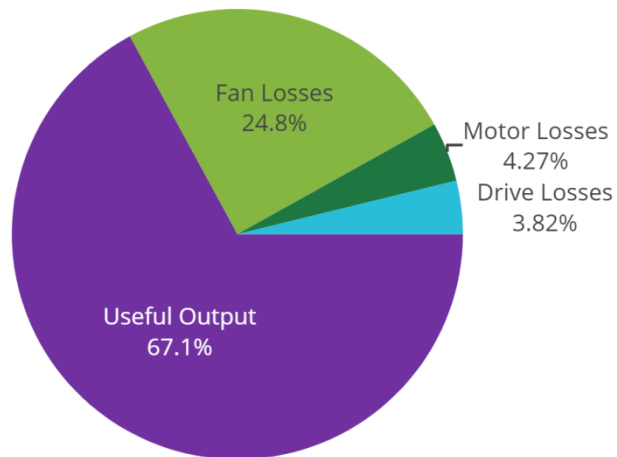
## Example assessment



Baseline conditions

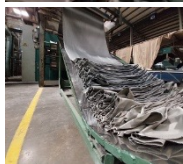
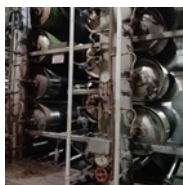


Optimized Fan & Motor Combo



Reduced Pressure & Flow

Source: MEASUR



# QUESTIONS?